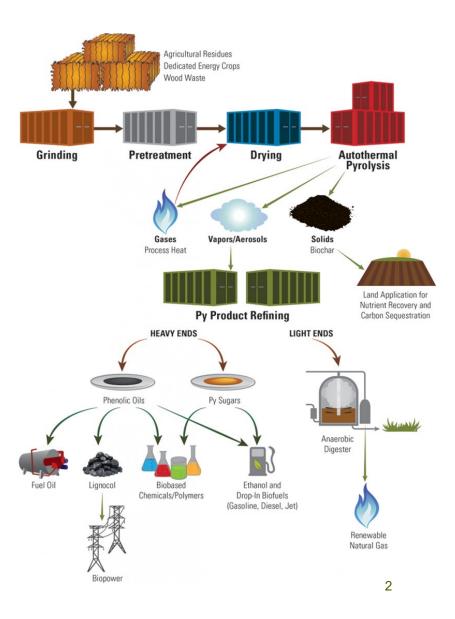
IOWA STATE UNIVERSITY Bioeconomy Institute

Selective Oxidation of Biochar During Autothermal Pyrolysis

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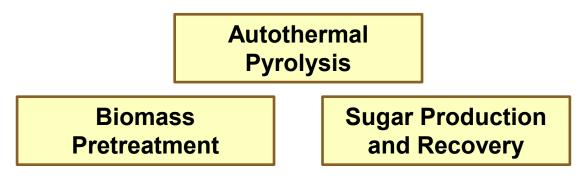
Vision for Biofuels and a Carbon Negative Economy

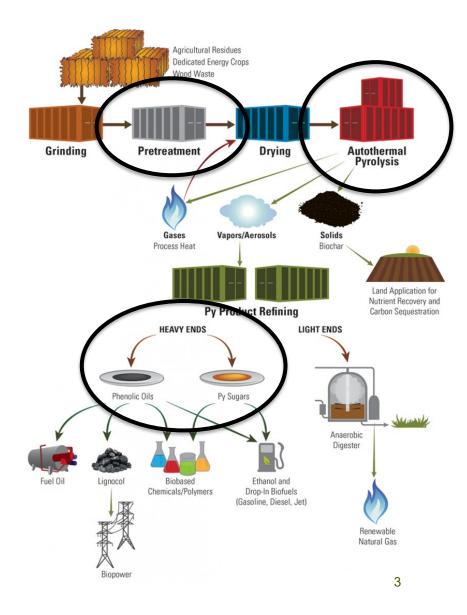
- The Bioeconomy Institute envisions a Carbon Negative economy through the pyrolysis of renewable resources for the production of biochar and renewable energy
- Optimize the production and recovery of pyrolytic sugars than can be upgraded to cellulosic fuels



Vision for Biofuels and a Carbon Negative Economy

- The Bioeconomy Institute envisions a Carbon Negative economy through the pyrolysis of renewable resources for the production of biochar and renewable energy
- Optimize the production and recovery of pyrolytic sugars than can be upgraded to cellulosic fuels
- <u>This Discussion</u>:





Autothermal Pyrolysis

 Conventional pyrolysis thermally decomposes organic compounds in the absence of oxygen to produce primarily liquids

Gasification

0.15 < Φ < 0.35

 Heat transfer limited process in overcoming endothermic reactions to provide enthalpy of pyrolysis (≈1 MJ/kg)

Autothermal

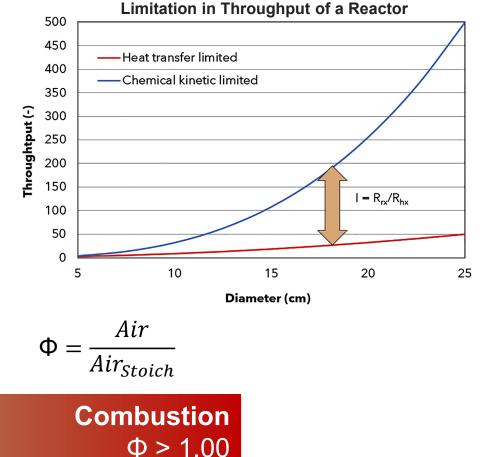
Pyrolysis

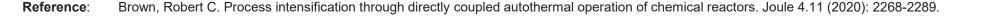
 $0.06 < \Phi \le 0.12$

Pyrolysis

 $\Phi = 0.00$

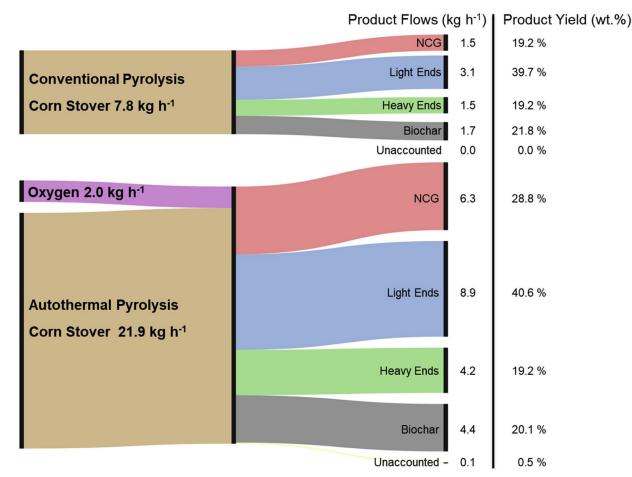
 Autothermal pyrolysis provides the energy for pyrolysis through partial oxidation of pyrolysis products within the reactor





Three-fold Process Intensification using ATP

 Removal of heat transfer bottleneck through autothermal pyrolysis increases biomass throughput up to three-fold



Autothermal Pyrolysis Advantages:

- Process intensification
- Simplified reactor design
- Full-blown air fluidization
- Reduced capital costs

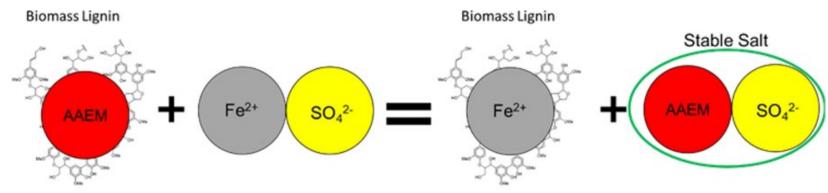
Enhanced Py Sugars with AAEM Passivation

- Passivation of alkali and alkaline earth metals (AAEM) with sulfuric acid pretreatment prevents fragmentation of pyranose and furanose rings
 - Increased sugar yields in an auger pyrolyzer at up to 250%
- Significant char agglomerations limit reactor operability
 - Passivation slows lignin decomposition resulting in melting



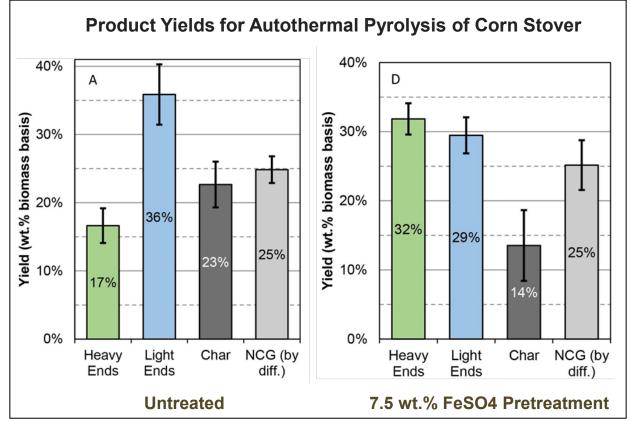
Char Agglomerations

• Developed ferrous sulfate pretreatment to enhance pyrolytic sugar formation and add a catalyst selective towards lignin depolymerization



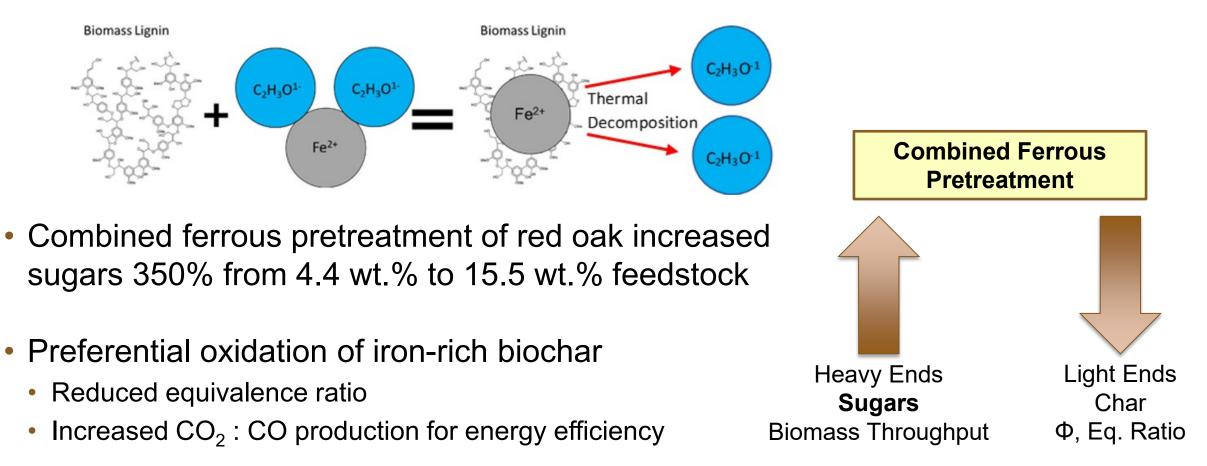
Ferrous Pretreatment Enhanced Sugar Production

- Ferrous sulfate pretreatment allows for continuous operation of conventional pyrolysis with comparable yields to acid pretreatments
- Autothermal pyrolysis of ferrous sulfate pretreated corn stover achieved volumetric sugar production ≈2040 gL⁻¹h⁻¹
 - 32 times higher than conventional pyrolysis
 - 10 times higher than acid pretreatment
- Low ash feedstock (red oak) still produced agglomerations at increased biomass throughputs



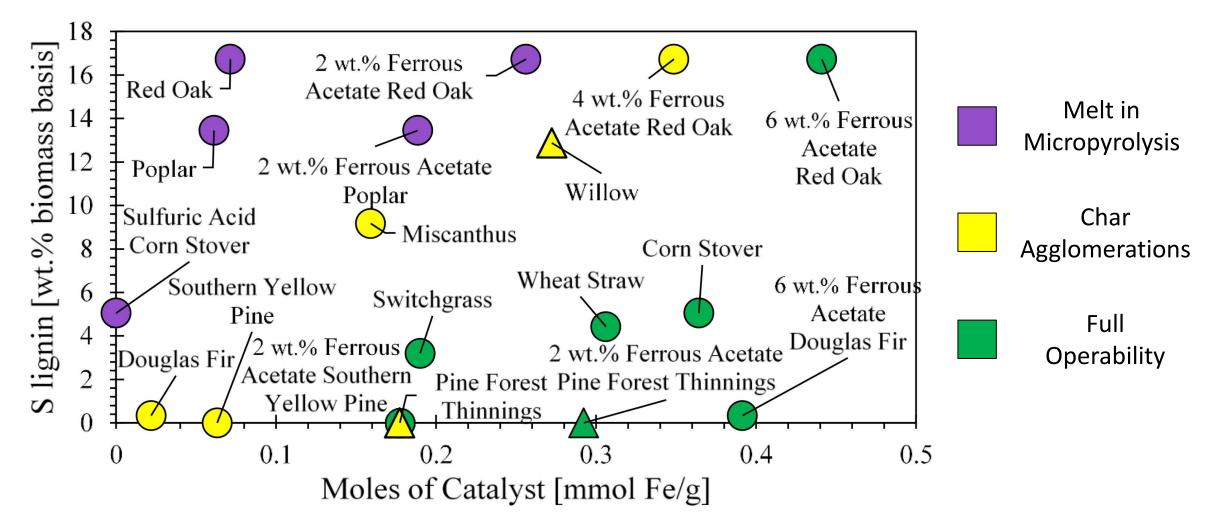
Enhanced Oxygen Utilization with Iron Infused Char

 Increase the loading of catalytically active ferrous cations in low ash feedstocks by pretreating with a ferrous salt



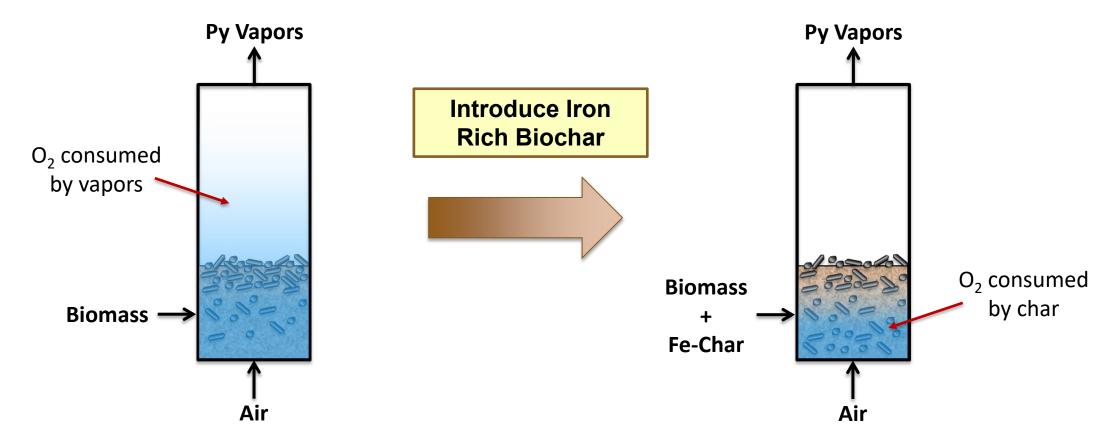
Ferrous Treatment Recipe to Continuous Operation

• Reactor operability depends on S-lignin content and catalyst loading



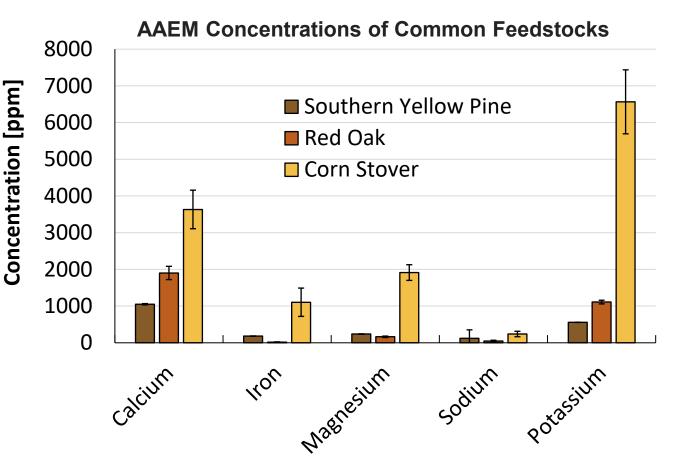
Proposed Selective Oxidation to Increase Py Sugars

- Introduce iron-rich char with biomass during autothermal pyrolysis to preferentially oxidize the char and provide the enthalpy of autothermal pyrolysis
- Minimize the oxidation of pyrolysis vapors to maximize sugar production



Southern Yellow Pine as Control Feedstock

- Southern yellow pine is low in ash content and S-lignin compared to other feedstocks
- Treat southern yellow pine with 2.0 wt.% Ferrous Acetate to produce ferrous-loaded char
- Co-feed 85 wt.% untreated southern yellow pine with 15 wt.% ferrous-char
- Autothermal conditions at 500°C and 1 kg/hr



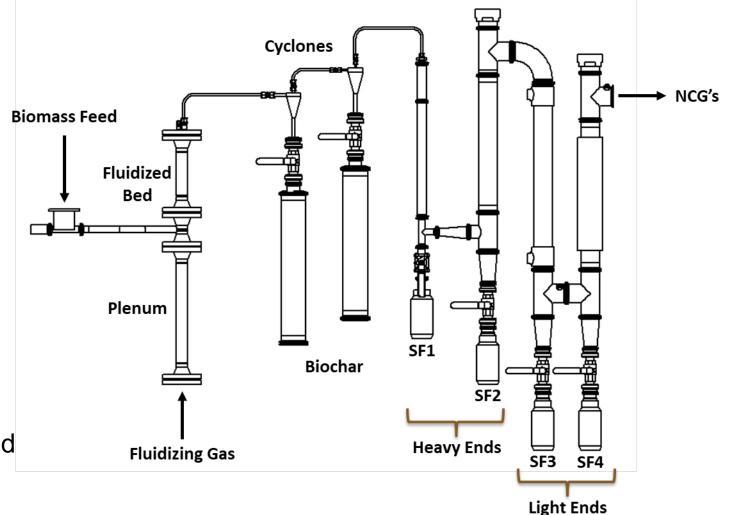
Continuous Production at the Laboratory Scale

Fluidized Bed Reactor:

- 3.81 cm (1.5 inches)
- Silica sand bed
- Conventional $\rightarrow N_2$
- Autothermal \rightarrow Air + N₂

Collection System:

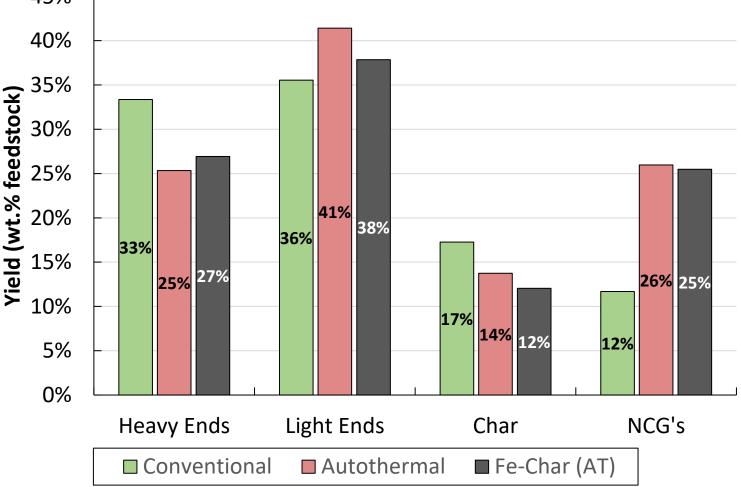
- Char removed via cyclones
- Hot condenser (SF1)
- Hot ESP (SF2)
- Cold Condenser (SF3)
- Cold ESP (SF4)
- Noncondensable gases quantified using micro-GC



>20% Increase in Sugars with Ferrous Loaded Char

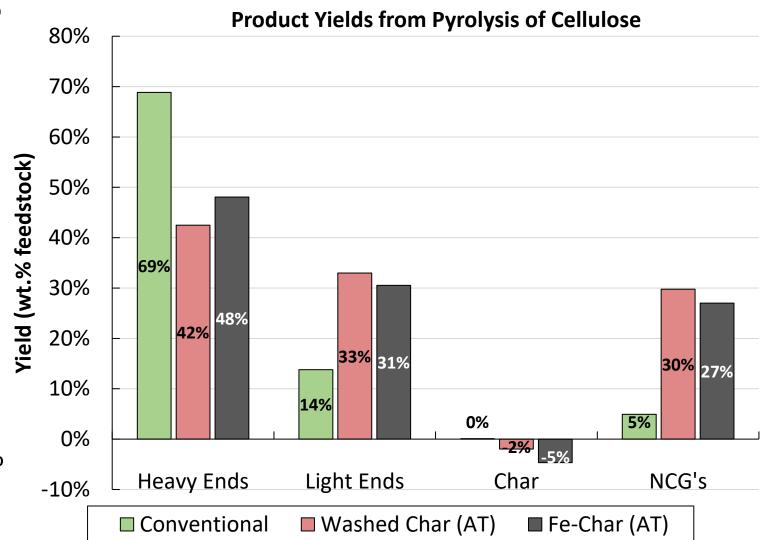
- Co-fed ferrous acetate char increased heavy ends and decreased light ends when compared to biomass only autothermal
- 22% increase in total sugars for autothermal:
 - Conventional = 7.2 wt.%
 - Autothermal = 5.4 wt.%
 - Fe-Char (AT) = 6.6 wt.%
- Decrease in char suggests
 improved char oxidation

Product Yields from Pyrolysis of Southern Yellow Pine



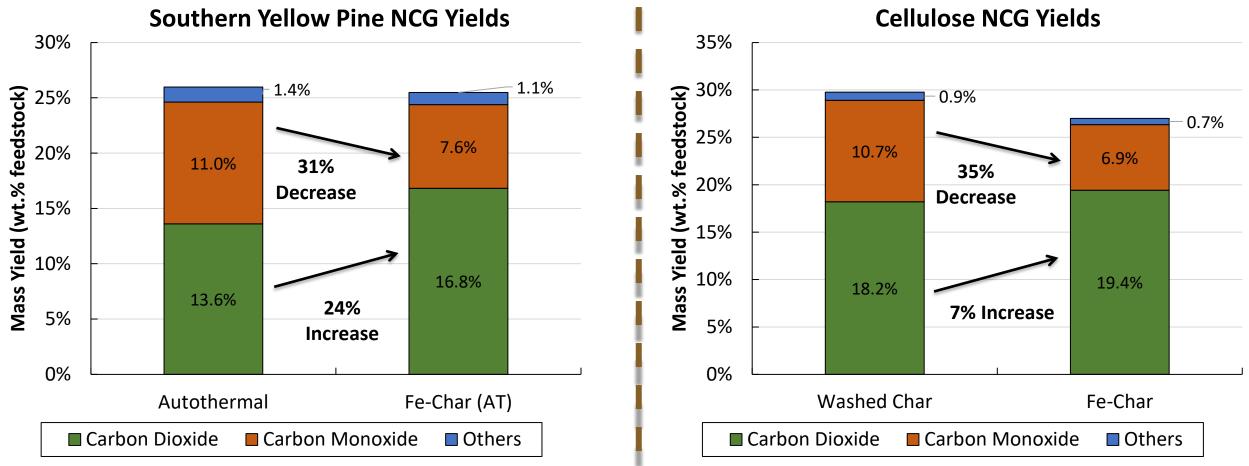
Cellulose co-fed with Char Supports Fe-Char Activity

- Co-fed cellulose at 85 wt.% with 15 wt.% char
 - Washed 1M HCl char
 - Fe-loaded char
- Direct comparison of catalyst loading char shows improved recovery of sugars
- Total Sugars:
 - Conventional = 61.3 wt.%
 - Washed Char (AT) = 32.1 wt.%
 - Fe-Char (AT) = 36.2 wt.%



CO₂ Yield Supports Preferential Char Oxidation

Ferrous loaded char boosted CO₂: CO ratios → releases more energy for less carbon



Conclusions

- Ferrous pretreatments of biomass enhance pyrolytic sugar production during autothermal pyrolysis.
- Co-pyrolysis with ferrous loaded char and untreated biomass promoted oxidation of char and preserved sugar production.
- Preferential oxidation of ferrous loaded char yields predominately carbon dioxide thus releases more energy during autothermal pyrolysis.
- Co-feeding ferrous loaded char and biomass can selectively oxidize char to further enhance pyrolytic sugar production.

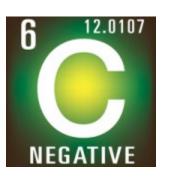
Acknowledgements

- Iowa State University's Bioeconomy Institute
 - Co-authors
 - Staff and students
- This research was funded in part by the US Department of Energy sponsored RAPID Institute.

- Be sure to catch our other talks/posters this week!
 - Demonstration Autothermal Pyrolyzer
 - Thermal-oxo degradation of plastics
 - Upcycling and pyrolysis of plastics







Questions?