Mid-size LNG design considerations for robust and flexible operation: Yangling LNG plant as a case study

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Yangling LNG presentation

- Owner : Shaanxi LNG Investment and Development Co LTD
- 0.5 MTPA LNG production
- Peak Shaving Plant
- Air Products AP-SMR[™] Liquefaction Process
- TPFMC in charge of the LNG train and storage facilities
 - Successfully started up and running since 2015



Design Challenges

- Flexibility to meet big fluctuations in gas quality and quantity
- Robustness and High efficiency at varying loads
- Operational flexibility for turn up and down
- Imported power
- Imported refrigerant: no in-situ fractionation

Feed Gas Quality

	Gas Source	
Feed component	А	В
Methane	95.7	92.88
Ethane	1.341	4.107
Propane	0.209	0.759
C4	0.0691	0.316
C5	0.0247	0.084
C6+	0.0124	C6+:0.089



Preteatment

- Liquefaction with AP-SMR technology
- Boil Off Gas recycled back to plant
- 2 x 25 000 m3 LNG tanks
- Additional LNG export by trucks



Key Parameter: Operating Pressure Pretreatment and Liquefaction

- Total Power decreases with pressure with an optimum at 77 bar
- Capital cost is reduced by optimizing the largest rotating machinery
- An increase in pressure in pre-treatment allows reduction in equipment and piping volume.
- A smaller MR compressor leads to smaller refrigerant inventory and imports vs increase in inlet compression

ease 120.0% 110.0% 100.0% 90.0% HorsePower 80.0% 70.0% 60.0% 50.0% as 40.0% 50 80 40 Natural Gas Pressure ----Overall GHP (kW)

Power versus Pressure at train inlet

Heavy Hydrocarbon Removal Three Routes

Phase Envelope



pressure

pressure

TSA (Temperature Swing Adsorption) at high pressure

Heavy Hydrocarbon Removal

A combined solution of Temperature Swing Adsorption (TSA) and Partial condensation are selected

- Maximise liquefaction operating pressure => limit capital cost
- HHC are a byproduct
- Flexible and versatile to treat different feedstocks
- Optimise the size of each component to minimise the capital cost



HHC removal: Reuse of Cooling Gas for Heating

- Optimisation of the TSA beds:
- 50 % reduction in regeneration gas
- Lower risk of thermal stress by limiting temperature variations at downstream equipment at the end of cooling



Feedstock Variation: Checking for Source C

Source C was provided late in the project, after procurement of main equipment, with large BTEX and C8+ content

- An in-depth study assessed the impact and additional features to maintain full production
- No significant impact to overall production
- Size of the TSA beds increased





Turndown

- Peakshaving plants must operate at low turndown for extended periods of time
- Yangling LNG turndown operation was checked in detail down to 40%: no opening of recycle valves observed
- Experience of stable operation below nominal turndown

Prolonged operation below 5% turndown during tank cooldown



Variable speed drive

- High Voltage Semiconductor VSI driven motor in operation
- Adjust production demand without venting costly refrigerants
- Minimize (and avoid) compressor recycling across operating window
- Ease of operation
- Restart from settle out pressure, thus avoiding venting of refrigerant
- Stable operation during hot summer days and cold winter days



Conclusions

A midscale plant brings big challenges:

- The design has to maximise profit when pipeline gas is available and at an early stage not all constraints are yet known
- Potentially wide range of fluctuations in HHC content in feed gas needs practical solution to overcome an apparent uncertainty for the life of the plant.
- Flexibility has to be built in to anticipate modifications at minimum cost
- Experience in the unique area of mid-scale LNG plant design helps avoiding surprises

Yangling LNG Project : Thanks

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Yangling LNG Plant Owner: Shaanxi LNG Investment and Development Co LTD 陕西液化天然气投资发展有限公司



