



TCBIOMASSPLUS 2019

October 7-9, 2019 | The Hyatt Regency O'Hare | Rosemont, IL

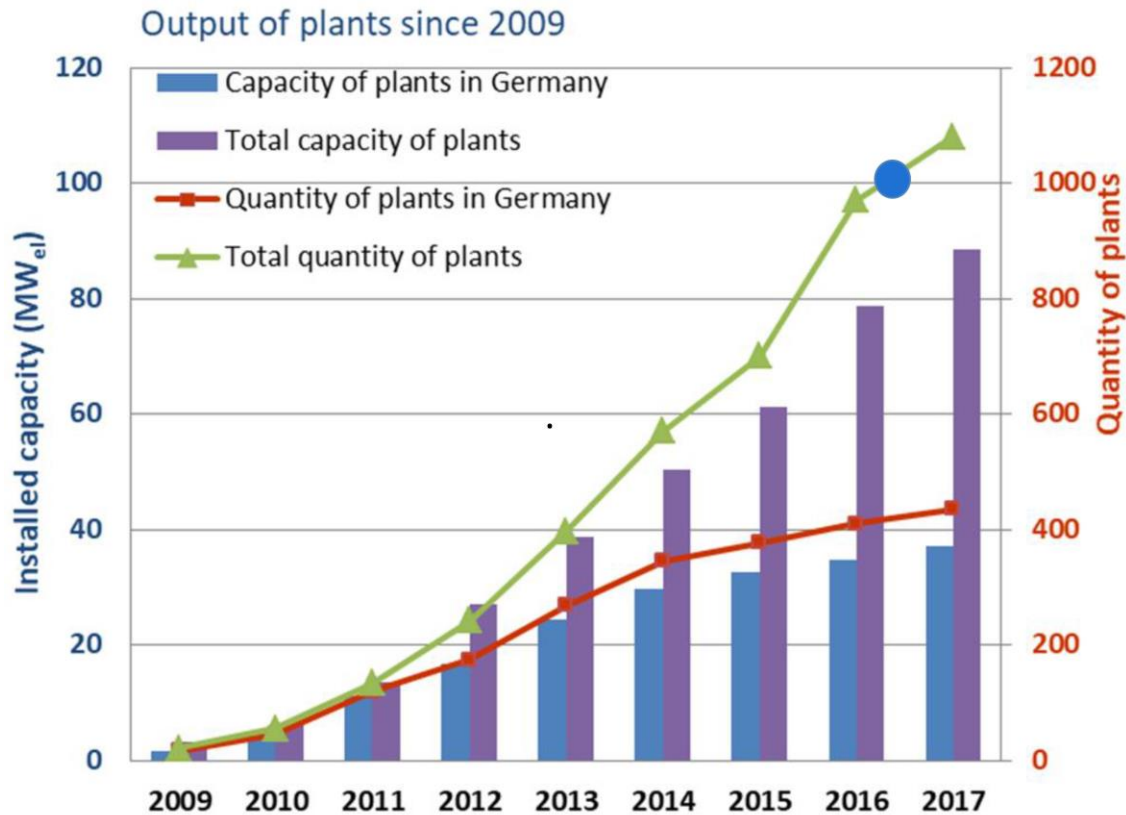
Small-scale Biomass Gasification CHP Systems: Comparative Performance Assessment and Char Valorization

Marco Baratieri

F. Patuzzi, D. Antolini, D. Basso, V. Benedetti, E. Cordioli



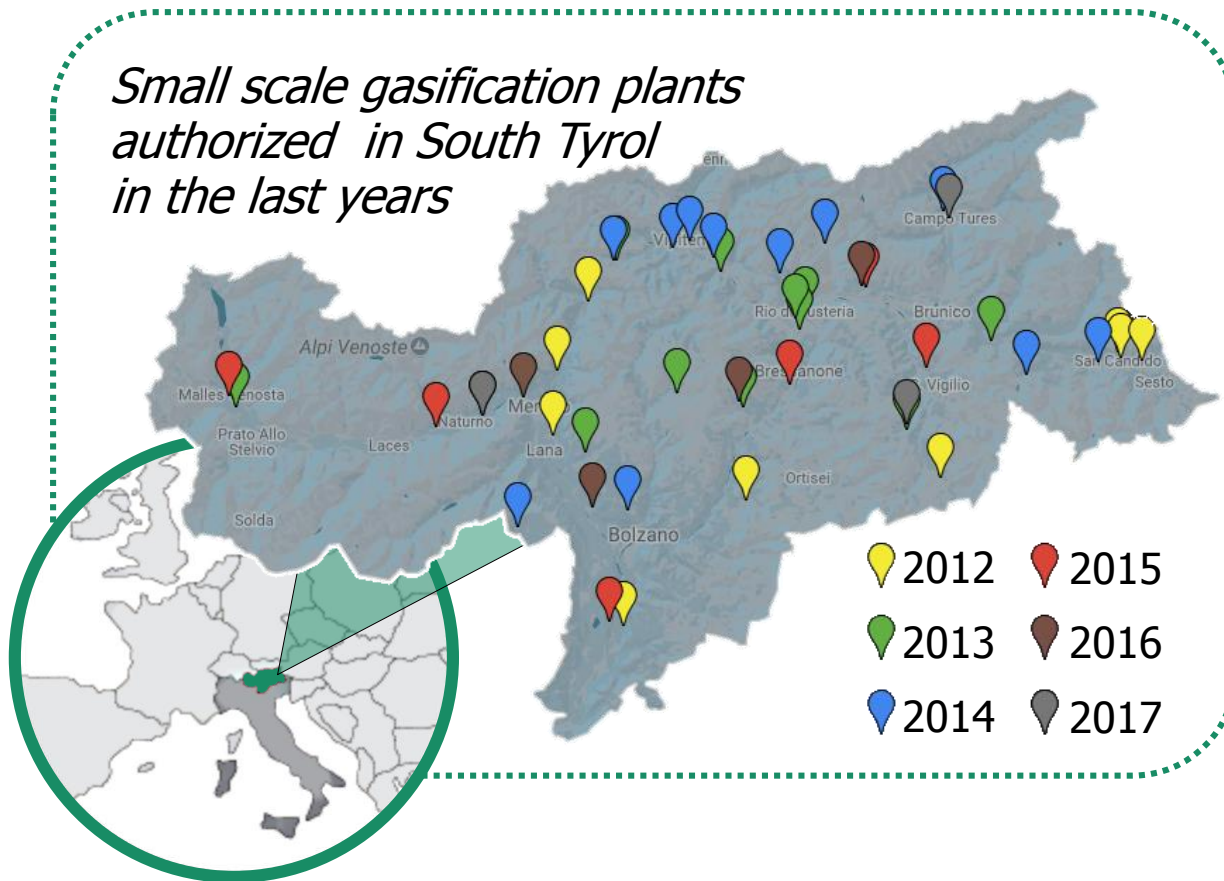
Small scale gasification: EU facts & figures



[D. Bräkow, 9. „Internationale Anwenderkonferenz Biomassevergasung“, 5. Dezember 2017 / Innsbruck]

Distribution of gasification plants in South-Tyrol

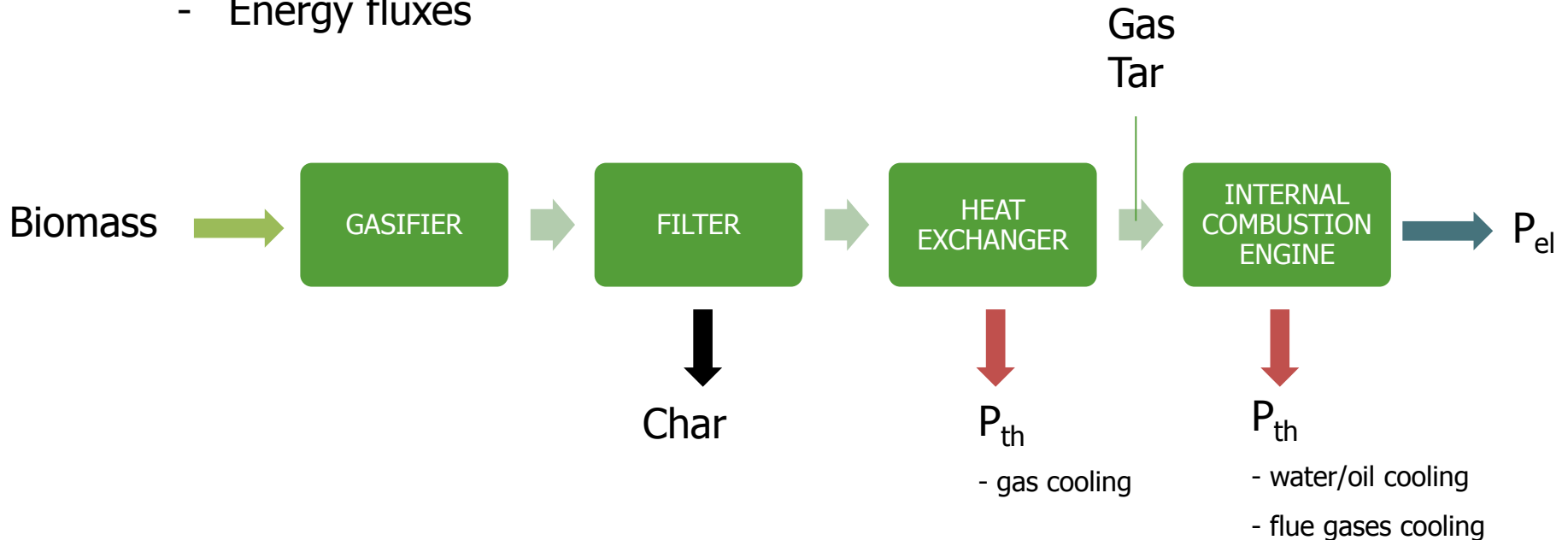
Small scale gasification plants authorized in South Tyrol in the last years



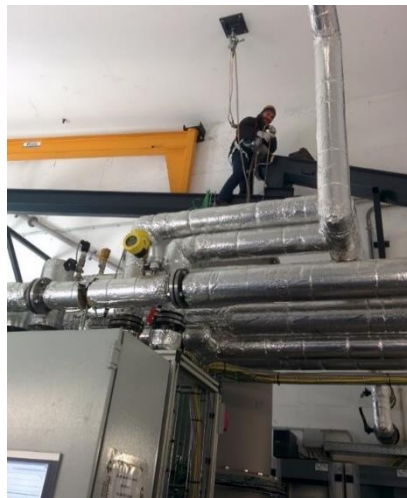
Outline of systems & monitoring activities

Analyzed parameters

- Feedstock and gasification products (gas, char e tar) characteristics
- Mass fluxes
- Energy fluxes



On site monitoring activities



Mass fluxes

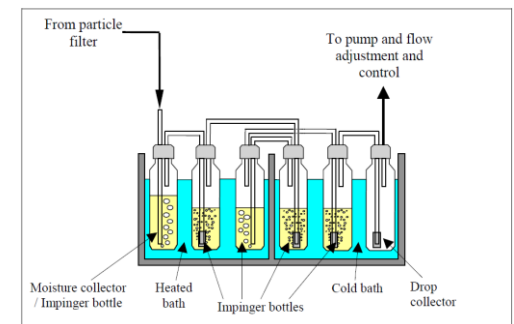
- Woody biomass flow rate
- Gasifying agent (air) flow rate
- Producer gas flow rate
- Char flow rate

Energy fluxes

- Input fuel
- Producer gas
- Power and heat

By-products characterization

- Liquid: tar
- Solid: char

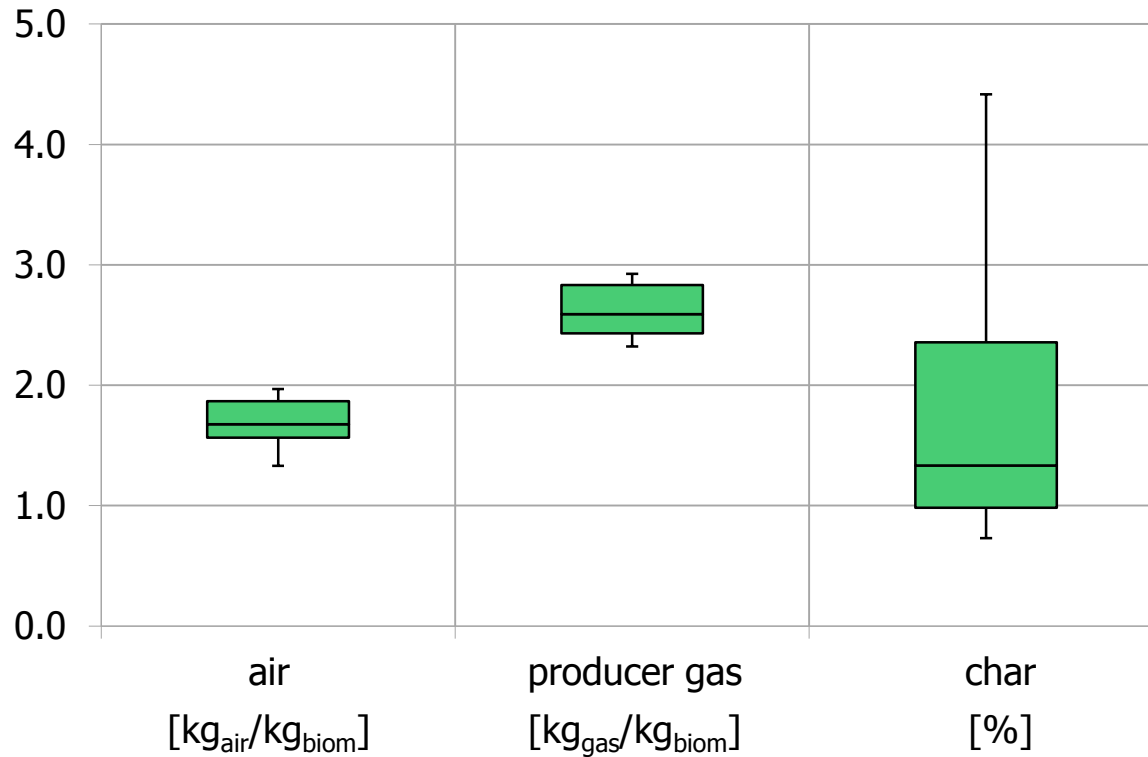


Mass balances of selected technologies

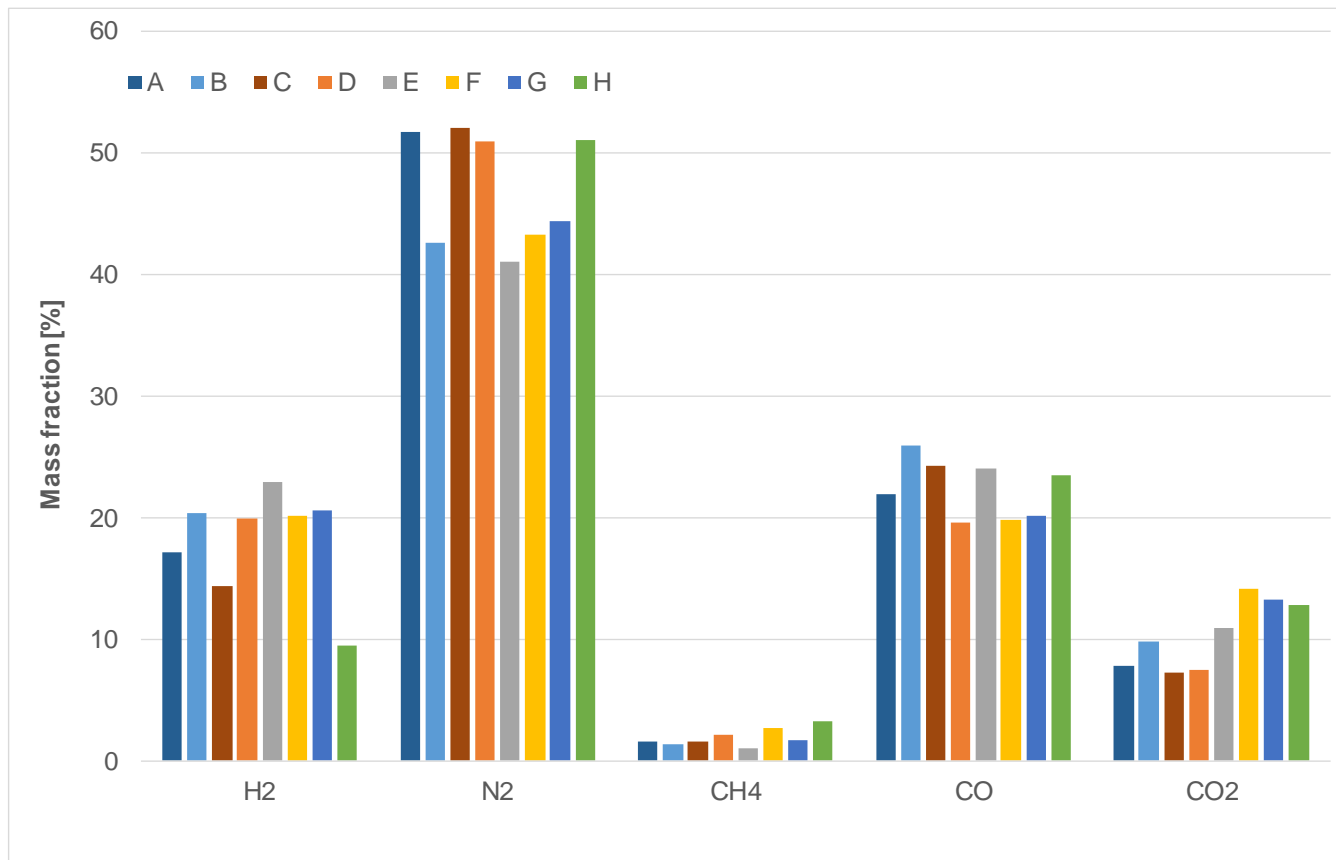
Technology	Dry biomass [kg/h]	Air [kg/h]	Producer gas [kg/h]	Char [kg/h]	Mass balance closure [%]
A	39.6	68.7	107.6	0.7	-
B	127.3	205.8	313.9	1.3	-5.4
C	116.9	155.6	271.4	1.1	-
D	123.8	185.0	297.6	5.1	-2.0
E	42.6	78.2	121.3	0.7	1.0
F	229.0	363.3	558.8	22.8	-1.8
G	338.4	663.0	990.4	3.6	-0.7
H	150.8	296.9	426.5	1.1	-4.5

Mass balance

variability (on considered technologies)

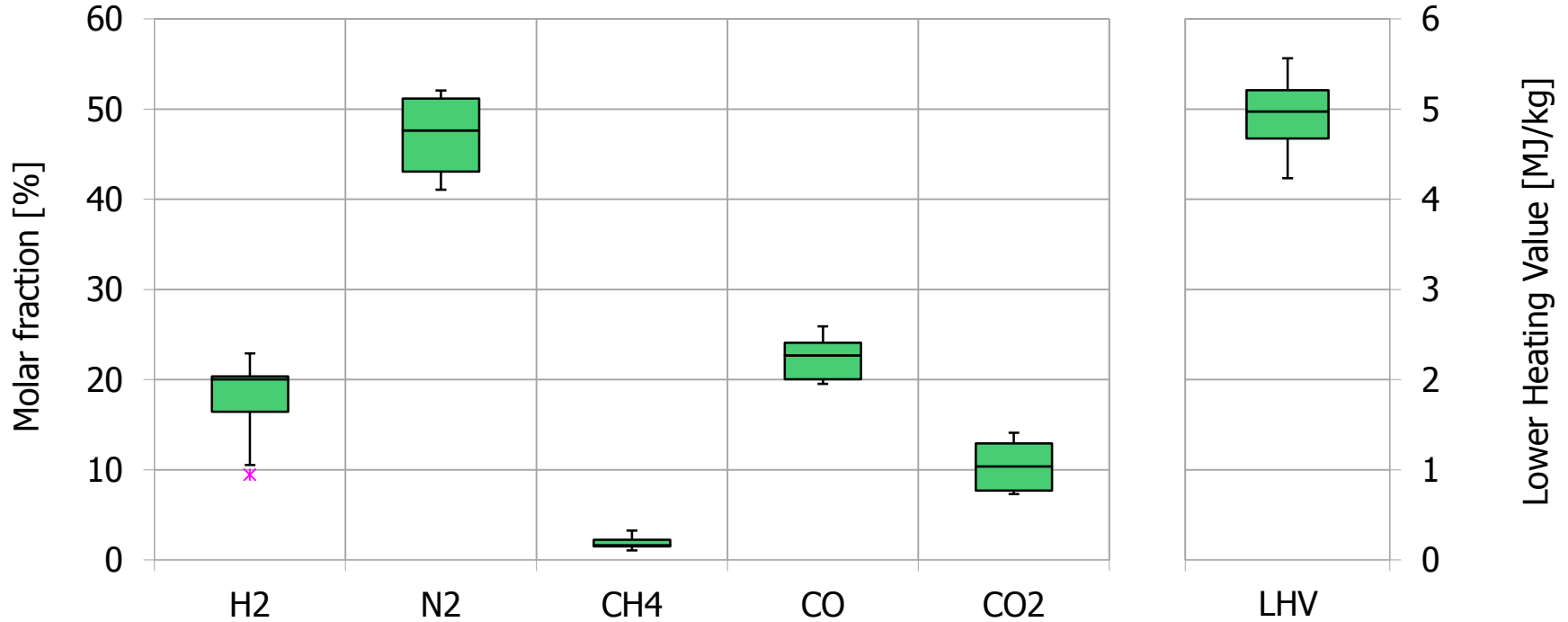


Producer gas composition



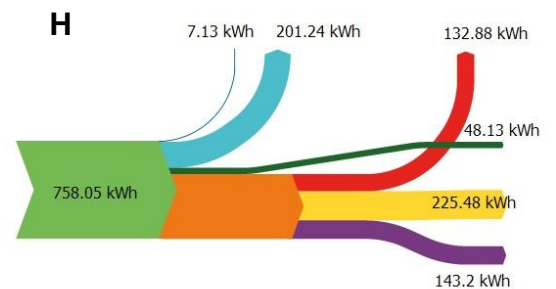
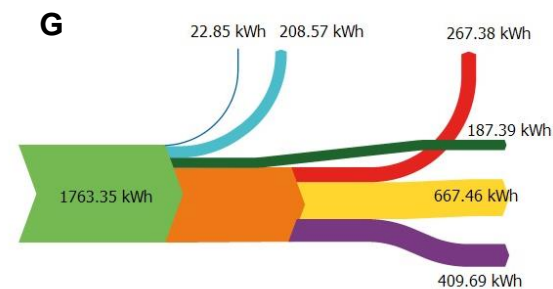
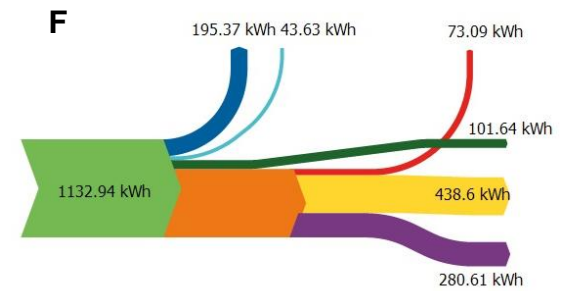
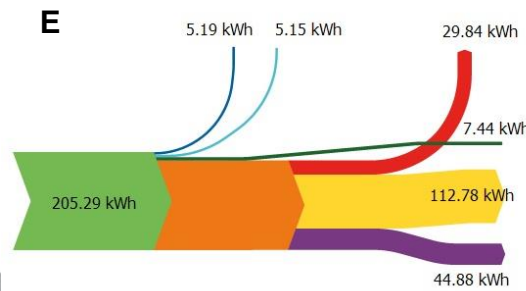
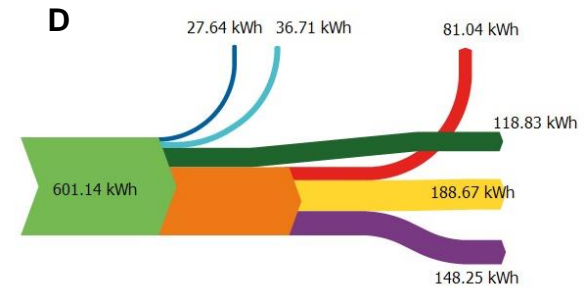
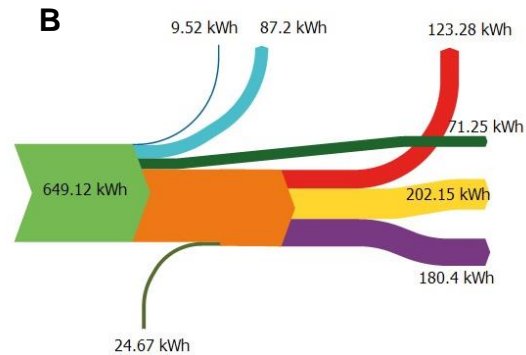
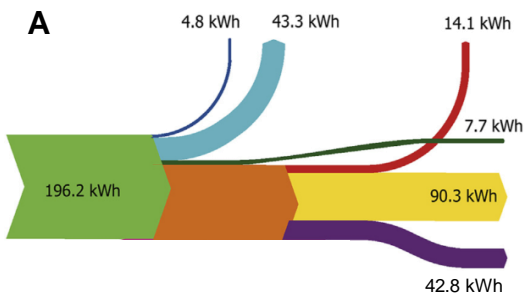
Producer gas composition

variability (on considered technologies)



Small scale gasification: b.o.p.

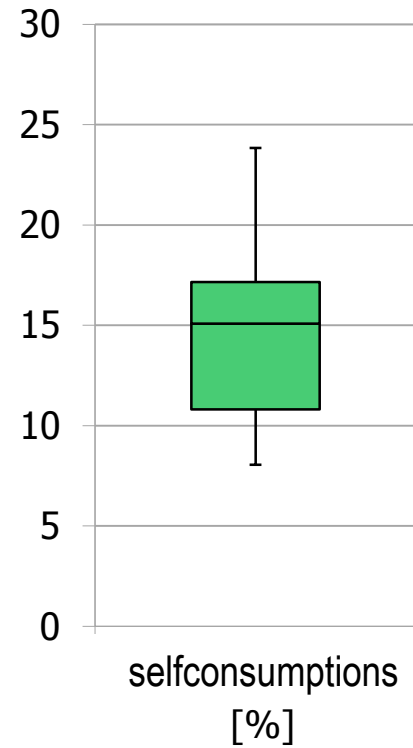
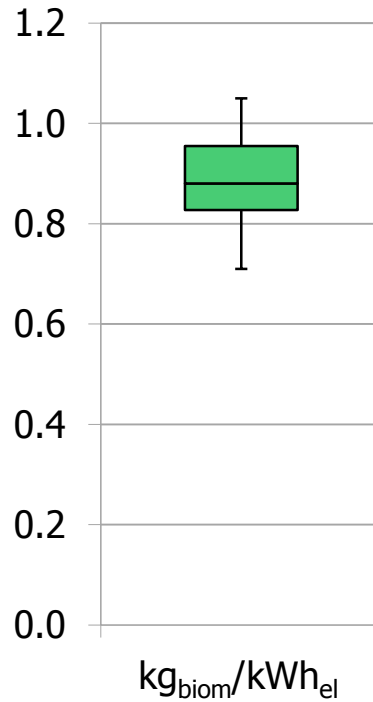
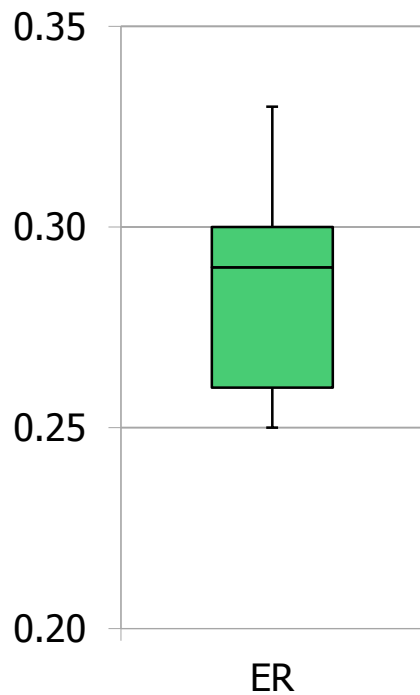
- Input biomass [kWh]
- ICE thermal output [kWh]
- ICE loss [kWh]
- Output char [kWh]
- ICE input [kWh]
- ICE electric output [kWh]
- Gasifier thermal loss [kWh]
- Gas-cooling thermal output [kWh]



Gasification performance parameters

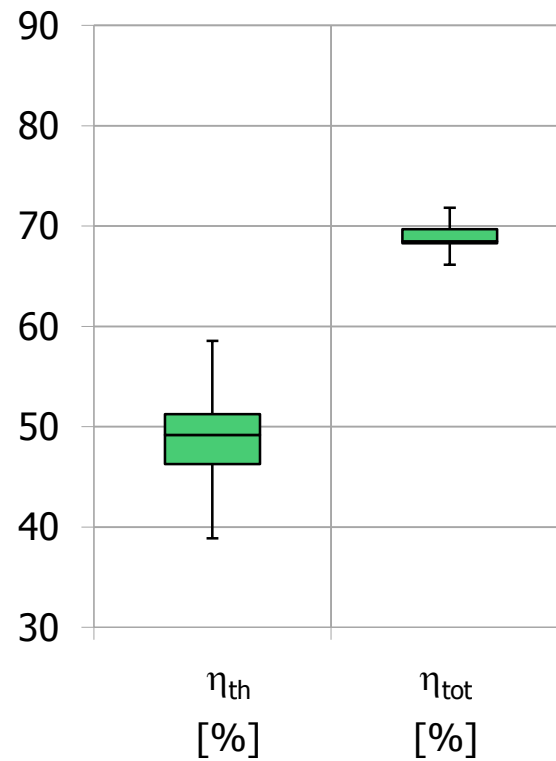
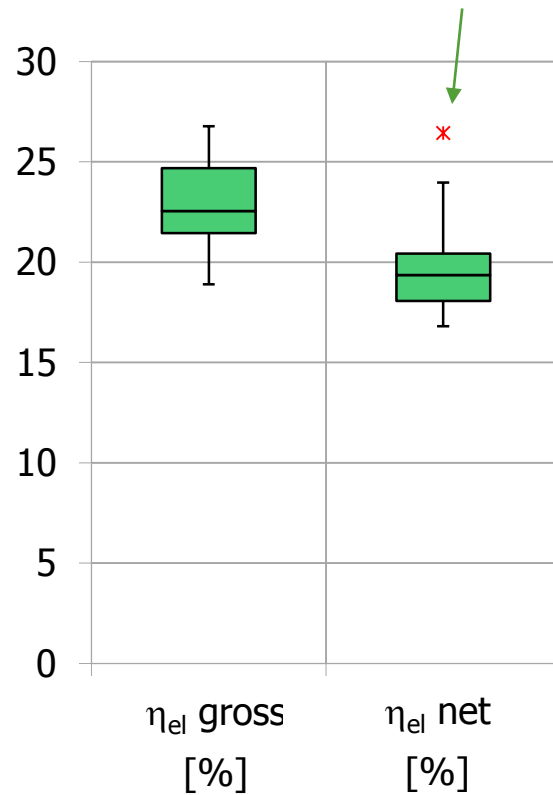
Technology	A	B	C	D	E	F	G	H
ER	0.30	0.26	0.29	0.25	0.29	0.26	0.33	0.30
η_{EL}	18.3%	26.4%	16.8%	18.8%	19.9%	21.9%	19.9%	17.4%
η_{TH}	49.9%	42.1%	52.5%	51.2%	58.6%	47.7%	48.5%	36.1%
η_{TOT}	68.2%	68.6%	68.3%	69.9%	78.5%	69.6%	68.4%	53.5%
kg_{BIOM}/kWh_{EL}	0.93	0.71	0.97	0.83	0.95	0.82	0.83	1.05

Characteristic parameters



Performance

Dual fuel engine (3 l/h of vegetable oil)



Char characterization



Technology	A	B	C	D	E	F	G	H
Ash [%]	27.84	16.08	49.52	31.50	13.34	6.49	29.17	25.64
C [%]	68.63	80.23	48.03	66.96	78.97	91.59	69.46	69.49
H [%]	0.33	0.49	0.89	0.18	0.68	0.52	0.11	0.20
N [%]	0.83	0.23	0.25	0.16	0.20	0.25	0.12	0.46
O [%]	2.37	2.69	1.31	0.57	6.50	0.60	0.87	3.88
LHV [MJ/kg]	23.04	26.64	14.33	19.65	25.38	30.81	22.84	24.12
PAH [mg/kg]	4881.4	2625.6	2.76	315.6	1223.5	85.6	31.43	441.2
PCB [mg/kg]	339.5	10.7	0.03	0.56	1.83	0.40	0.20	107.8

BET [m ² /g]	352	128	78	281	587	272	320	306
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Small scale gasification: feedstock (critical issues).

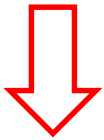
- ✓ Very low moisture content: < 10%
 - Vs direct combustion: 15-20%
 - need of a dryer
 - ✓ Constant characteristics
 - homogeneous granulometry (e.g. chips, pellets)
 - constant typology (wood)
 - very few (no) finer presence
- ↓
- ✓ Biomass higher cost: approx. 130 – 150 € / ton
Vs direct combustion 70 – 80 € / ton



Small scale gasification: char (critical issues).

✓ Char management

- char screw conveyors extract hot char from the gasifier, so they are subjected to deformation and breakage
- char management and storage is often problematic because it is a very light material and easily transportable by air



- ### ✓ High disposal cost: approx. 200 – 400 € / ton



Small scale gasification: gas cleanup (critical issues).

Pollutant	Example	Problems	Method
Particulate	Ash, char	Erosion	Filtration, scrubbing
Alkali	Na, K compounds	Hot corrosion	Cooling, condensation, filtration, adsorption
Nitrogen	Mainly NH ₃ , HCN	NO _x formation	Scrubbing, SCR
Tar	Aromatic compounds	Filters clogging, combustion problems, deposits, catalysts poisoning	Removal, condensation, thermal/catalytic cracking
Sulfur, Chlorine	Mainly H ₂ S, HCl	Corrosion, gaseous emissions, catalysts poisoning	Scrubbing, with dolomite or lime, adsorption



Small scale gasification: others (critical issues).

- ✓ Autonomy and control of the system
 - low degree of automation, i.e. problems lead to complete shut down of the system; time to restore the operation
- ✓ Feeding system: (screw conveyors):
 - blockage/distortion for presence inhomogeneous or inert material or different woodchips geometry
- ✓ Reactor and air nozzles
 - high temperature can melt steel components
 - higher T values than expected ones
 - reactors must be periodically opened and cleaned to remove inert materials



Challenges for gasification

short term

CHP upgrade

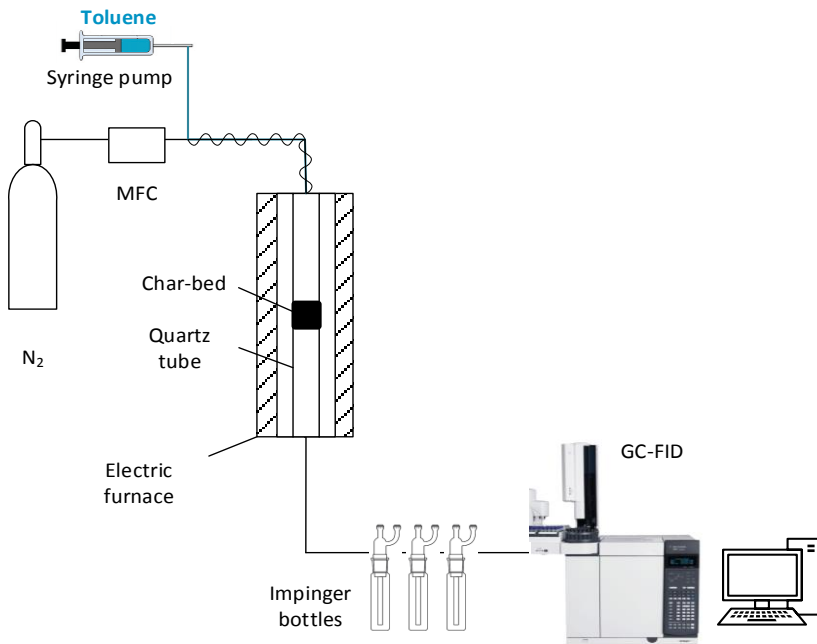
- fuel flexibility
- partial load operation
- char utilization
 - . filtering medium (ACS subs.)
 - . catalyst

medium term

CHP → POLYGENERATION

- biofuels
- hydrogen
- SNG
 - . PtG (Power2gas / CO₂ capture)
 - . integration with other renewables

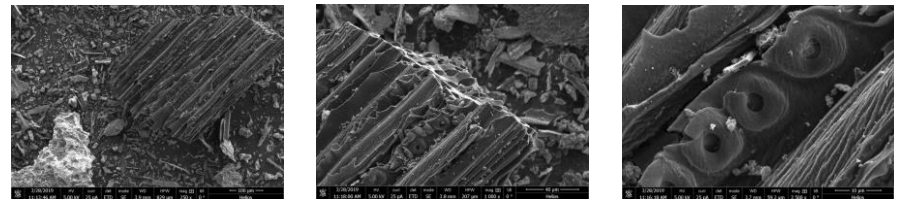
Use of char: tar cracking



Cordioli et al., *Energies* (2019)

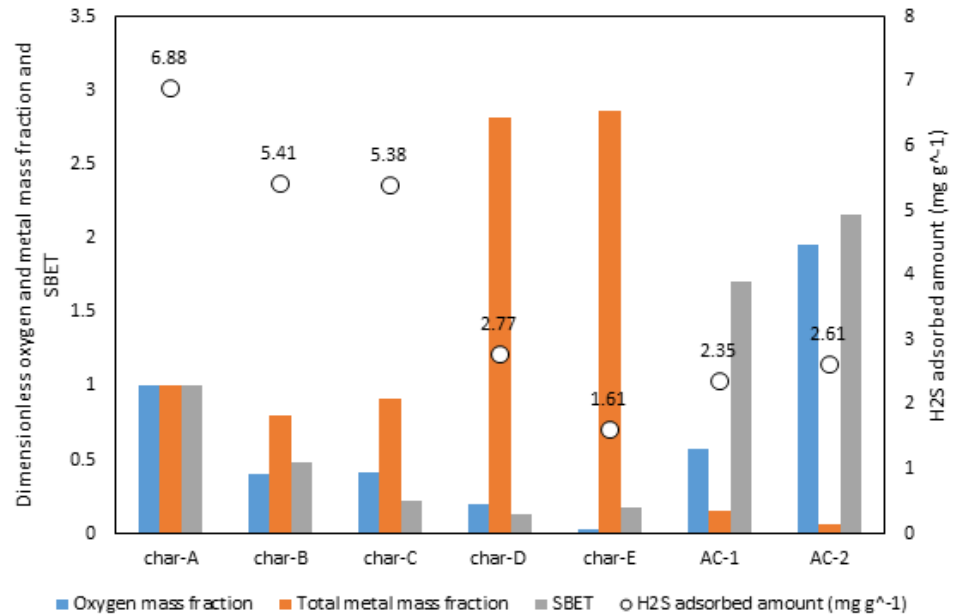
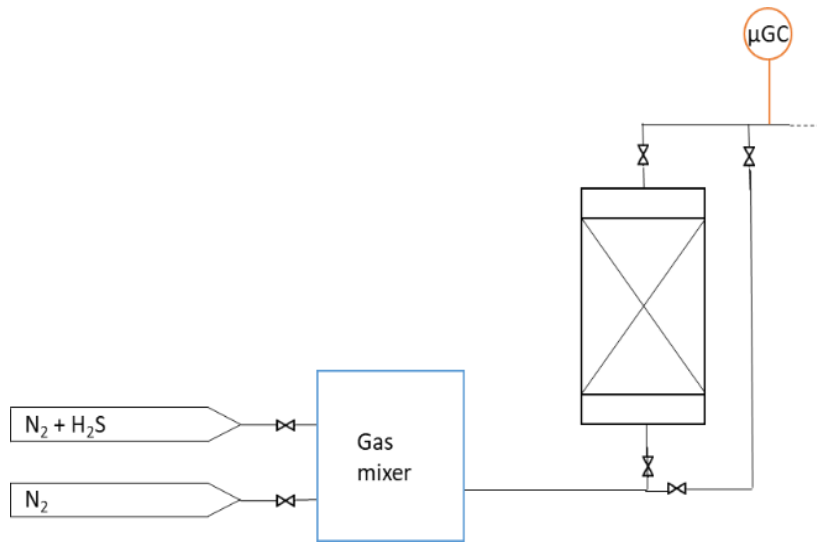
Plant type	Dual stage gasifier
Feedstock	Wood chips
Proximate and ultimate analysis	
	[wt% _{dry}]
Ash	22.20
C	78.97
H	0.68
N	0.20
S	0.31
HHV _{dry} [MJ/kg]	25.53
S _{BET} [m ² /g]	587
Pore volume [cm ³ /g]	0.30

Ash composition	
Mass fraction	
	[%]
Ca	17.47
Mg	2.18
Fe	1.12
P	0.84
Mn	0.56
Na	0.40
Al	0.38
S	0.37
Cr	0.30
Ba	0.22



	Empty-reactor tests		Tests with char-bed	
	900 °C	1000 °C	900 °C	1000 °C
Toluene removal efficiency [%]	39.9	97.3	60.3	99.0

Use of char: adsorption



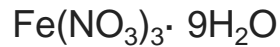
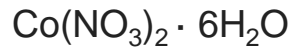
Marchelli et al. (2019)

Benedetti et al. (2019)

Use of char: catalyst support for FT synthesis

Catalysts

Precursors:



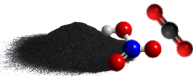
Supports:



Char



HNO₃ treated char






CO₂ activated, HNO₃ treated char



Commercial activated carbon

Method: Incipient wetness impregnation

	CO conv., %
 CO	Char, 20% Co 2.6
 H ₂	AC, 20% Co 27.7
 Ar	Literature 15 – 80
	Char, Fe 26



- Fixed-bed reactor
- H₂ : CO = 2 : 1
- T = 240°C
- P = 16 bar
- WHSV = 3600 ml g⁻¹ h⁻¹
- t = 24 – 72 h

Towards advanced biofuels: polygeneration

Renewable Energy Directive II (RED II)

Renewable transport fuels target: 14% (3.5% advanced b.)

SET plan & Action 8 Implementation plan

Gasification is a key technology in 3 (of 7) value chains

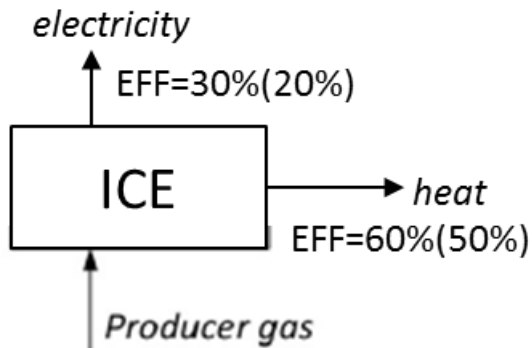
required: efficiency improvement, 30%, GHG savings, 60%
cost reduction, to 50 (2020) – 35 (2050) €/MWh

Strategic Research and Innovation Agenda (ETIp, EERA Bioenergy)

Major role for gasification value chains in agreement with SET pl.

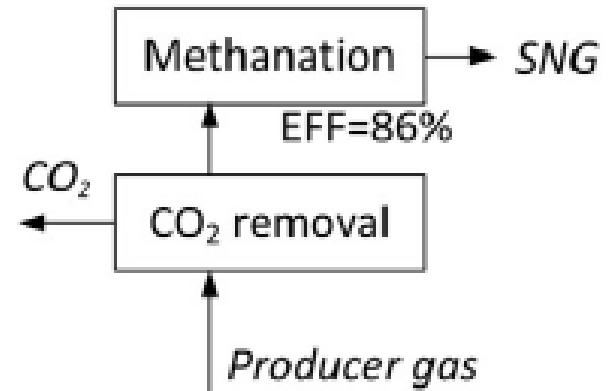
Polygeneration

Today (... almost yesterday)

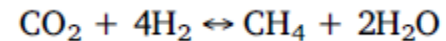


Saric et al., *Journal of CO₂ Utilization*, 20 (2017) 81-90

Tomorrow (... almost today)

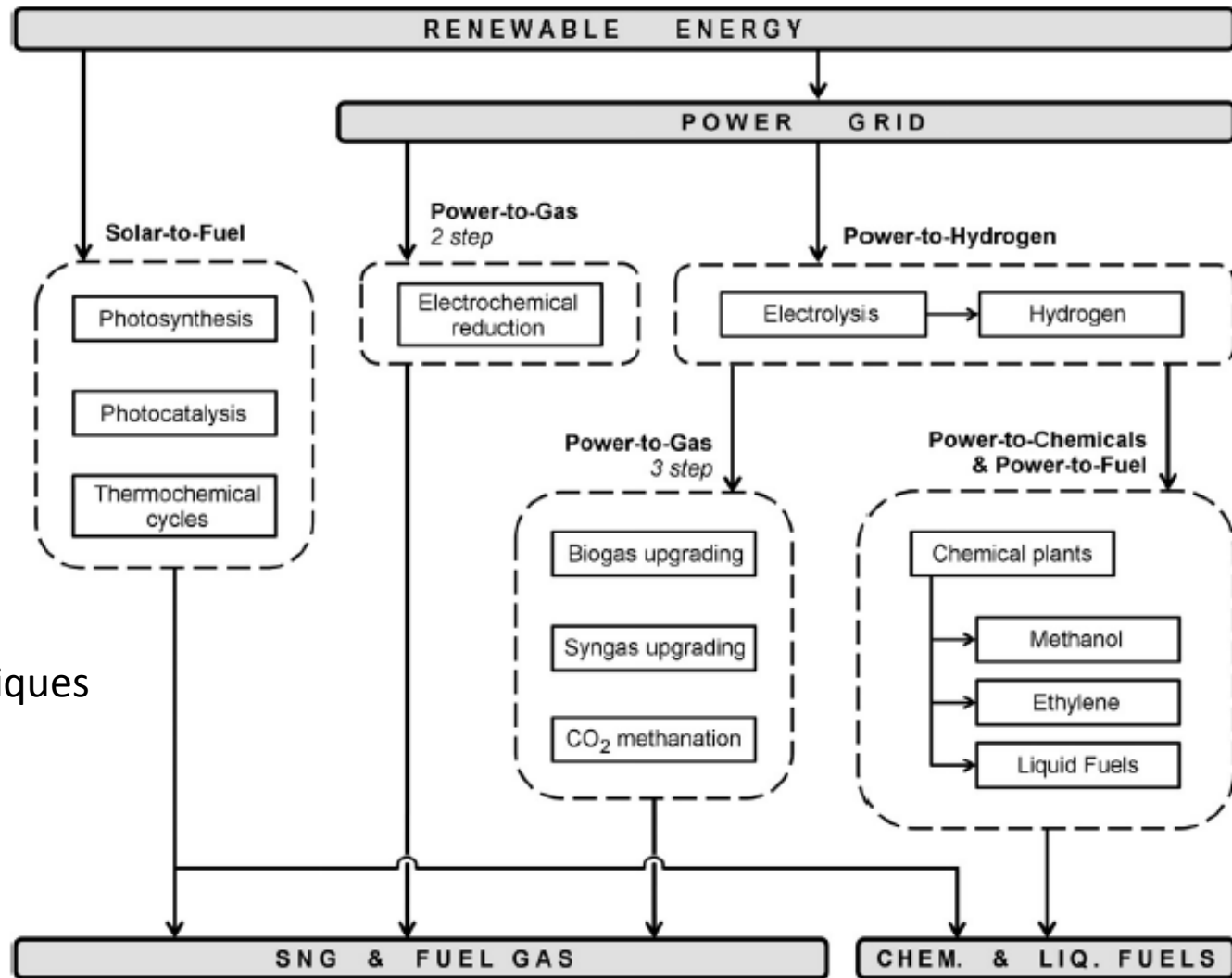


Sabatier reaction



$$\Delta H = -164.9 \text{ kJ/mol}$$

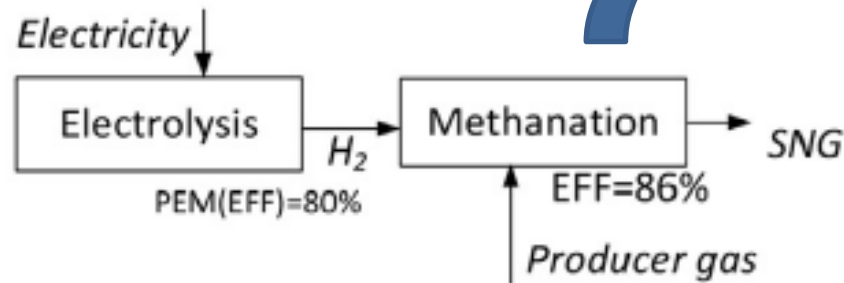
Power-to-gas (PtG)



Renewable energy and CO₂ hybrid storage techniques

Power-to-gas (PtG) and gasification

Tomorrow (PtG)



Saric et al., Journal of CO₂ Utilization, 20 (2017) 81-90

Tomorrow (biomethanation)



Syngas fermentation

Menin et al. (2019)



Remarks: main directions for gasification

- **Increase fuel flexibility** [use of low-cost feedstock]
- **Use char as co-product** [(!) legislative framework]
- **Co-production of fuels/chemicals/materials** [poly-generation]
- **Combining thermochemical and biochemical processes**
- **Optimization of resource efficiency** [wind, solar, hydro]

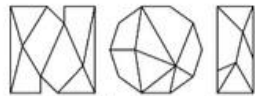
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